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TURBULENCE AMPLIFICATION WITH INCIDENCE AT THE LEADING EDGE OF A COMPRESSOR CASCADE

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ABSTRACT

Detailed measurements, with a two-component laser-Doppler velocimeter and a thermal anemometer were made near the suction surface leading edge of Controlled-Diffusion airfoils in cascade. The Reynolds number was near 700,000, Mach number equal to 0.25, and freestream turbulence was at 1.5% ahead of the cascade.

It was found that there was a localized region of high turbulence near the suction surface leading edge at high incidence. This turbulence amplification is thought to be due to the interaction of the free-shear layer with the freestream inlet turbulence. The presence of the local high turbulence affects the development of the short laminar separation bubble that forms very near the suction side leading edge of these blades. Calculations indicate that the local high levels of turbulence can cause rapid transition in the laminar bubble allowing it to reattach as a short "non-burst" type.

The high turbulence, which can reach point values greater than 25% at high incidence, is the reason that leading edge laminar separation bubbles can reattach in the high pressure gradient regions near the leading edge. Two variations for inlet turbulence intensity were measured for this cascade. The first is the variation of maximum inlet turbulence with respect to inlet-flow angle; and the second is the variation of leading edge turbulence with respect to upstream distance from the leading edge of the blades.

NOMENCLATURE

C	= chord length
p	= pressure
q^2	= $u'_i u'_i$, twice energy of turbulence
Re	= chord Reynolds number
S	= distance along the chord
Tu	= turbulence intensity, $\sqrt{u'^2 + v'^2} / V_{ref}$
U	= tangential velocity
u'	= tangential fluctuating velocity
V	= axial velocity
v'	= axial fluctuating velocity
V_{ref}	= upstream reference vel., $\sqrt{U^2 + V^2}$ upstream
V_{tot}	= local total velocity, $\sqrt{U^2 + V^2}$
x	= tangential direction
y	= axial direction
β_1	= inlet flow angle
ν	= kinematic viscosity

INTRODUCTION

While experimental research was being conducted on the Sanger cascade blades at high inlet-air angles in the cascade wind tunnel of the Naval Postgraduate School (Sanger and Shreeve, 1986), complementary calculations, which were initially unsuccessful, were performed in an attempt to predict the off-design performance. Flow visualization studies by Sanger and

Shreeve, at chord Reynolds number of 340 000, indicated the presence of a laminar separation bubble near the leading edge. The cascade geometry was documented in Elazar and Shreeve (1989), and was the same geometry used for the calculations. The viscous flow features of this cascade are shown in Figure 1.

Testing by Hobson and Shreeve (1993) indicated that at a very high inlet-flow angle ($\beta_1 = 48.4^\circ$) the turbulence intensity right at the leading edge was amplified for the Sanger cascade. This could explain how a laminar separation bubble would be able to reattach as a short bubble in the steep pressure gradient near the leading edge at high incidence.

A deeper understanding of this phenomenon is desirable so as to correctly compute the boundary layer development in the leading edge, especially for compressor blading operating near stall. This is not only true for relatively simple inviscid-viscous methods, but also for full Navier-Stokes calculations. To gain a greater understanding of this phenomenon, detailed LDV measurements were made in the leading edge region of the Sanger cascade for inlet-flow angles of $\beta_1 = 43.3^\circ$, 46.4° and 48.4° . The order of magnitude of the leading-edge turbulence amplification, which was significant at high incidence, was confirmed by thermal anemometer measurements at $\beta_1 = 48.4^\circ$.

DESCRIPTION OF THE PHYSICS AND ANALYSIS TECHNIQUE

An inviscid-viscous scheme was used for the subsonic calculations (Martensen, 1954, LeFoil, 1965 and Roberts 1975). It was found that during the calculation the inviscid-viscous method predicted a "burst" laminar separation

bubble very near the leading edge for $\beta_1 \geq 38^\circ$, while the data of Sanger and Shreeve indicated the presence of a short bubble. Figure 2 shows a schematic of a short laminar separation bubble. A short laminar bubble "bursts" into a long bubble when reattachment is not possible in the short state, see Fig. 3 (for a description of the flow regimes possible with varying Reynolds number see, Roberts, 1975). As can be seen from Fig. 4 the suction surface velocity distribution is reasonably well predicted by the inviscid code. Since a long or "burst" laminar separation bubble by definition causes a significant change from the inviscid velocity distribution, which results in a decrease in the suction peak, this implies that the bubble present on the blade will be short.

As stated above the application of the boundary layer method predicted that the leading edge laminar separation bubble would not reattach. The Reynolds

number and freestream turbulence intensity ($Tu = 1.5\%$) were taken from upstream test conditions as given by Elazar and Shreeve (1989). The inviscid-viscous method was calibrated by Roberts (1975) for short and long mid-chord laminar separation bubbles, and for freestream turbulence intensities between ~ 0 to 5%. The method has been successfully applied to short bubbles found near the leading edge of a large chord wing model ($\sim 1.2\text{m}$) of a NACA 66₁3-018 section, which was experimentally measured by Gault (1955) in a low turbulence wind tunnel.

The only mechanism that affects transition in a laminar bubble, for a fixed geometry and Reynolds number, is the local turbulence level. The length of the laminar part of the bubble is decreased for an increased value of local free stream turbulence. Therefore, very high local turbulence could cause rapid transition after separation allowing short bubble reattachment even in a severe pressure gradient.

Additional calculations were performed for $\beta_1 = 40^\circ$, 43.3° and 46.4° and compared to the laminar bubble reattachment locations reported by Sanger and Shreeve (1986). These were determined from flow visualization studies performed at a Reynolds number of 340 000. For the calculations the experimental velocity distributions was used for the three inlet-air-angles mentioned above. This was done to ensure that the laminar boundary layer was properly calculated so as to correctly locate the laminar separation point.

At first the free-stream turbulence of $Tu = 1.5\%$ was used in the calculations resulting in the prediction of "burst" bubbles. The turbulence level was then increased in subsequent calculations until short bubble reattachment occurred for each inlet air angle. Finally, the turbulence level was further increased until the reattachment location agreed with the experimental data. This is shown in Fig. 5 where the turbulence required to match the data is indicated: $Tu = 8.5\%$ for $\beta_1 = 40^\circ$, $Tu = 9.0\%$ for $\beta_1 = 43.3^\circ$ and $Tu = 11.0\%$ for $\beta_1 = 46.4^\circ$. Not only does this indicate that at medium to high incidence the leading edge turbulence is amplified, but that the level of turbulence is also a positive function of incidence.

TEST FACILITY AND INSTRUMENTATION

The experiments were performed in the Low Speed Cascade Wind Tunnel (LSCWT) at the Turbopropulsion Laboratory of the Naval Postgraduate School, which is shown schematically in Fig. 6. For a more detailed description of the facility see Sanger and Shreeve (1986). The LDV measurements were performed with a two-component system, which is fully described by Elazar and Shreeve (1989). Fig. 6 also shows the location of the introduction of seeding into the bellmouth of the tunnel,

the profile coordinates of the Sanger Blade, and the cascade geometry and inlet conditions.

A 20 μm (sensor diameter) hot-film probe, which had a sensor length of 1 mm, was used with a TSI single channel hot-wire anemometer system (IFA-100 and -200) connected to a Personal Computer. A complete description of the hot-film instrumentation is given by Wakefield (1993)

EXPERIMENTAL PROCEDURE

Inlet pitchwise LDV surveys were performed ahead of the leading of the blades for three different inlet flow angles (43.3, 46.4 and 48.4 degrees). The six axial locations of the survey planes and respective orientation of the LDV were the same as those described by Hobson and Shreeve (1993). In their study, they performed detailed measurements upstream, downstream and through the passage of the blade row including around the leading edge separation bubble at the high inlet flow angle of 48.4 degrees.

Hot-film surveys were performed at the three survey planes which were closest to the leading edge of the blades (2.17, 1.10 and 0.57% axial chord ahead of the leading edges). The hot-film probe was positioned horizontally in the tunnel (i.e. in the tangential direction, with respect to the blades, with the sensor parallel to the spanwise direction) whilst traversing across the leading edges. This was done to ensure that there was no probe stem interference on the measured turbulence level as it was traversed past the leading edge.

RESULTS AND DISCUSSION

As can be seen from Figs. 7, 8 and 9, the locus of points of maximum turbulence intensity, for all three inlet flow angles considered, approaches the blade leading edge at right angles to the approaching stagnation streamline. The approximate location of the stagnation streamline is shown as the locus of points of minimum total velocity.

Due to small blade setting angle errors ($< 0.1^\circ$) and the lack of perfectly two-dimensional inlet flow there were small differences in trajectories of the maximum turbulence and minimum total velocity from blade to blade. However the overall trend as the locus of points approaches the blades is periodic.

The increase in turbulence intensity, ahead of the blade leading edge, is not due to streamwise diffusion, but is caused by local shear as the flow attempts to accelerate around the leading edge. Local shear will produce turbulence, as is shown by the production term in the transport equation for turbulent kinetic energy (Hinze 1975);

$$\frac{D}{Dt} \left(\frac{q^2}{2} \right) = - \frac{\partial}{\partial x_i} u'_i \left(\frac{p}{\rho} + \frac{q^2}{2} \right) - \overline{u'_i u'_j} \frac{\partial \bar{U}_j}{\partial x_i} + \nu \frac{\partial}{\partial x_i} u'_i \left(\frac{\partial u'_i}{\partial x_j} + \frac{\partial u'_j}{\partial x_i} \right) - \nu \left(\frac{\partial u'_i}{\partial x_j} + \frac{\partial u'_j}{\partial x_i} \right) \frac{\partial u'_i}{\partial x_j}$$

where the second term, on the right hand side, is the work by the viscous shear stresses of the turbulent motion or the production term.

A bi-cubic spline was fitted to the individual components of the LDV data in the pitchwise direction. This then allowed the differentiation of the measured velocity field, to determine each of the components of the two-dimensional production term.

$$\text{Prod.} \propto 2 \left\{ \left(\frac{\partial U}{\partial x} \right)^2 + \left(\frac{\partial V}{\partial y} \right)^2 + \left(\frac{\partial U}{\partial y} \right) \left(\frac{\partial V}{\partial x} \right) \right\} + \left(\frac{\partial U}{\partial y} \right)^2 + \left(\frac{\partial V}{\partial x} \right)^2$$

The distribution of measured turbulence production is shown in Fig. 10 for $\beta_1 = 48.4^\circ$. A "ridge" of high turbulence production exists in the region ahead of the blades, at right angles to the stagnation streamline and parallel to the points of maximum turbulence intensity. The significant turbulent production is the reason for the increase in turbulence ahead of the blades, particularly at increasing incidence.

Next the actual increase in turbulence intensity along the line of maximum intensity is plotted for each of the three test cases (see Fig. 11). As can be seen for all three the test cases, the increase is exponential and highly localized around the leading edge. Note that the hot-film probe measurements verify the turbulence level measured by the LDV system.

Furthermore in Fig. 12 the maximum turbulence intensity as measured by the LDV is plotted for each of the three inlet flow angles. Here the increase in maximum turbulence intensity is also seen to increase non-linearly, with increasing slope for increasing inlet flow angle. Note that the trend of increasing turbulence intensity with increasing incidence is similar to that of the data match of Fig. 5. However; the data presented is from a surface flow visualization at lower Reynolds number, while that of Fig. 12 has been measured by both LDV and a hot film approximately 1% of chord ahead of the leading edge.

Finally, the variation of turbulence intensity along the blade suction surface is given in Figure 13. The values in this figure are LDV measurements taken in the freestream at the edge of the boundary layer at midspan and plotted

in the streamwise direction. It can be seen that the turbulent boundary layer downstream of the laminar bubble develops in an elevated turbulence intensity environment that varies from approximately 12% near the leading edge to approximately 4% at the trailing edge. This is much higher than the inlet freestream value of 1.5% and this will have a significant effect on boundary layer development.

CONCLUSIONS

The experiments reported herein show that the free stream turbulence can be amplified greatly near the leading edge of a compressor blade at medium to high incidence angle. This increased turbulence level can have a strong effect on the boundary layer transition process, especially when conditions allow the formation of a laminar separation bubble.

The reasonable prediction of transition through a laminar bubble requires at least a reasonable assessment of the turbulence environment approaching the leading edge. For laminar bubbles occurring near the leading edge of compressor blades at high incidence, as well as the continued development of the turbulent boundary layer, the amplification of free stream turbulence should be taken into account in order to perform an accurate calculation of these flow phenomena. Also, the variation of elevated turbulence levels over the blade surface will affect boundary layer development downstream of the bubble and should be taken into account.

Finally, large scale experiments should be performed to better define the flow phenomenon of laminar bubbles and turbulence amplification at the leading edge suction surface of compressor blades at off design incidence and over the downstream surfaces.

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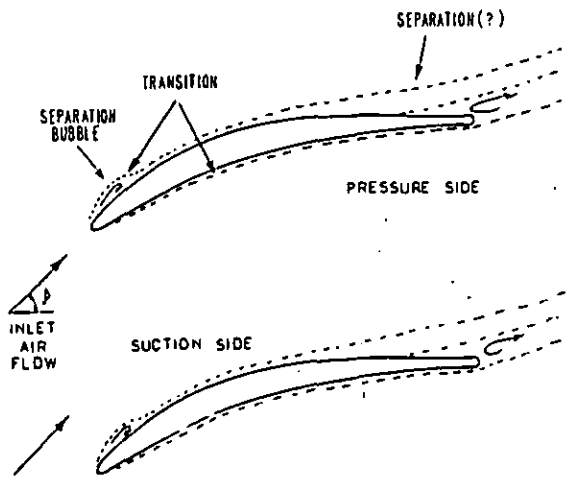
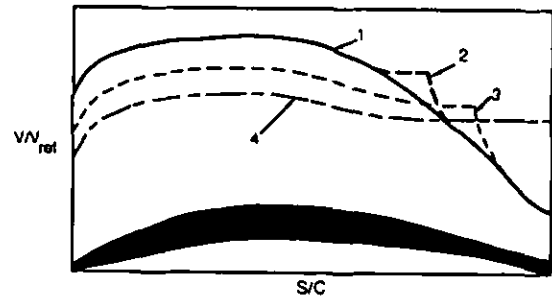


Fig. 1, Viscous Flow features of the Sanger cascade (Elazar and Shreeve, 1989)



- 1- High Re: No separation, velocity distribution approximates inviscid distribution
- 2- Medium Re: Short separation bubble, distribution approximately inviscid outside bubble region
- 3- Low Re: Long bubble after bursting, distribution significantly affected
- 4- Lower Re: Long bubble with complete separation

Fig. 3, Schematic of four flow regimes possible with varying Reynolds number over the suction surface of a compressor profile (Roberts, 1975)

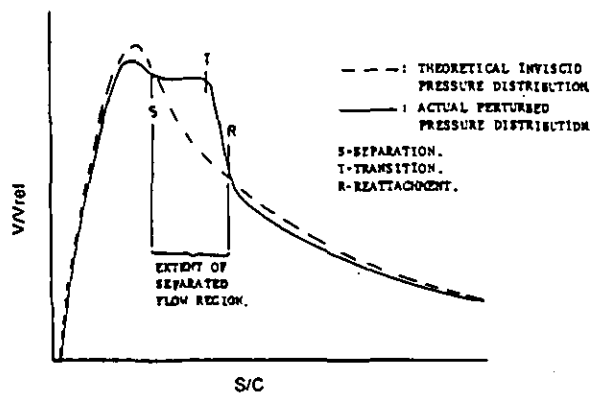
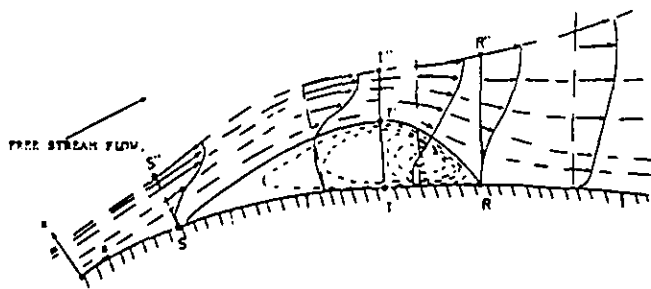


Fig. 2, Sectional view of a two-dimensional short laminar separation bubble and corresponding surface velocity distribution

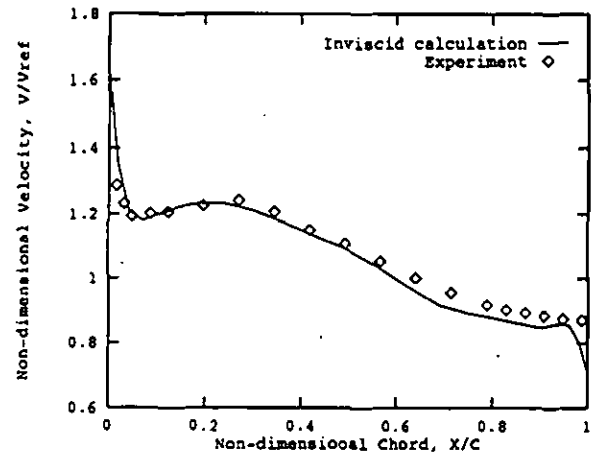


Fig. 4, Suction surface velocity comparison $\beta_1 = 40^\circ$

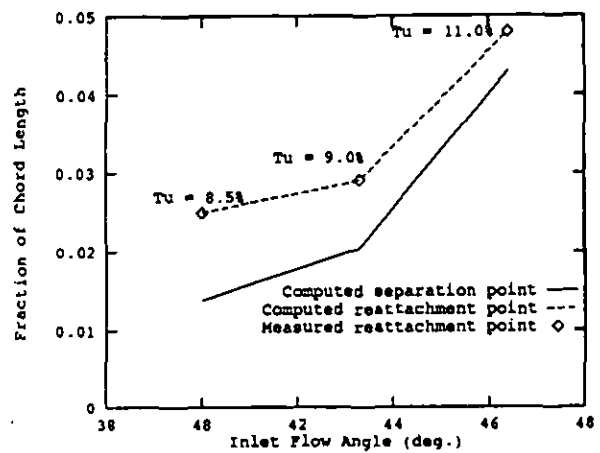
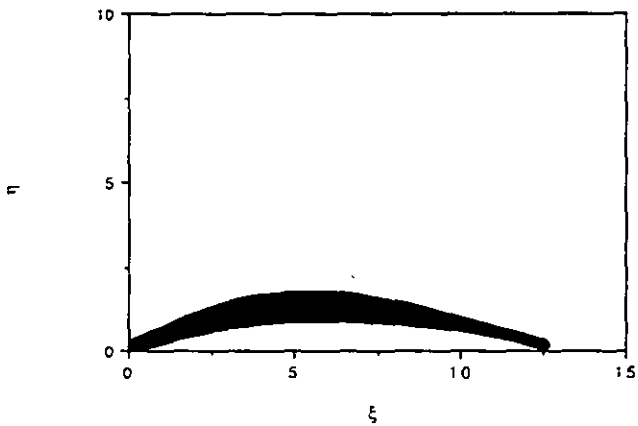
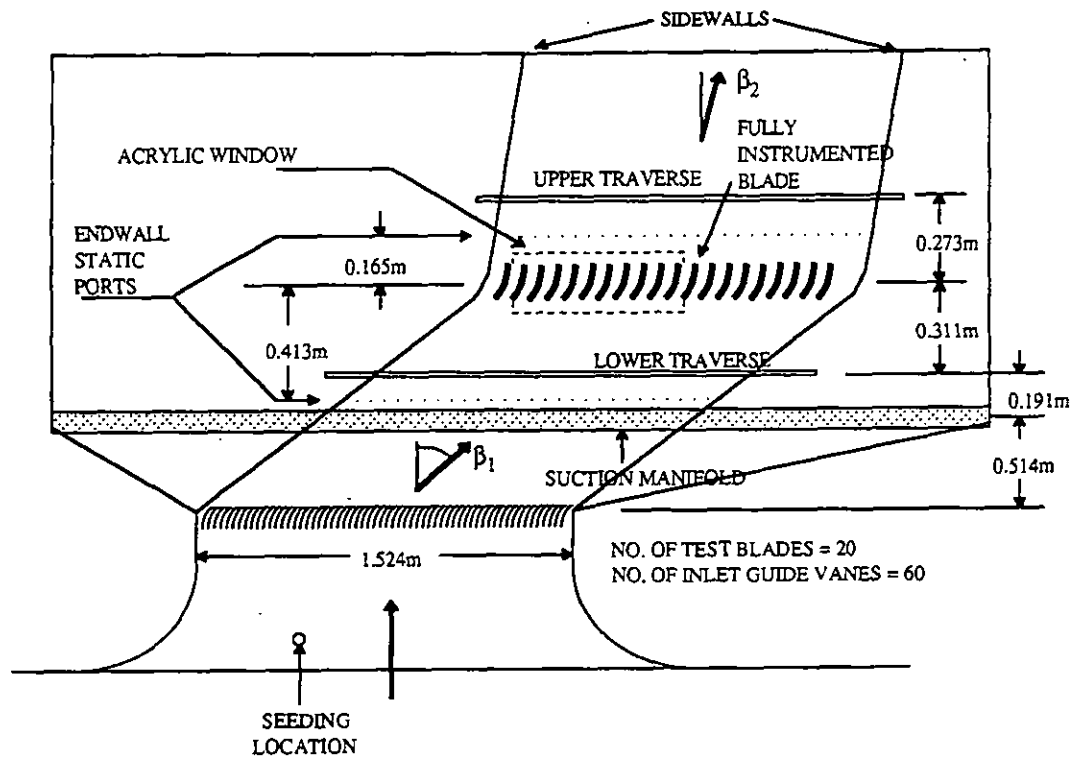


Fig. 5, Separation bubble reattachment for various turbulence intensities (Re = 340 000)



ξ	r (press. side)	r (suct. side)	
(mm)	(mm)	(mm)	Blade Type Controlled Diffusion
0.00	0.114	0.114	Number of Blades 20
0.56	—	0.213	Blade Spacing 76.2 mm
0.145	0.005	—	Chord 127.3 mm
0.564	0.112	0.498	Solidity 1.67
1.128	0.257	0.780	Leading Edge Radius 1.14 mm
1.692	0.394	1.024	Trailing Edge Radius 1.57 mm
2.256	0.526	1.240	Thickness 7%
2.819	0.648	1.425	Setting Angle $14.2^\circ \pm 0.1^\circ$
3.383	0.759	1.577	Stagger Angle $14.4^\circ \pm 0.1^\circ$
3.947	0.838	1.684	Span 254 mm
4.511	0.889	1.755	
5.075	0.912	1.791	TEST CONDITIONS
5.639	0.912	1.798	Reynolds No. 700,000
6.203	0.894	1.781	(Chord)
6.767	0.869	1.730	Inlet
7.330	0.841	1.651	Total Temp. 294 K
7.894	0.805	1.549	Total Press. 1.03 ATM
8.458	0.765	1.430	Mach Number 0.25
9.022	0.714	1.295	Freestream Turbulence 1.5%
9.586	0.653	1.151	
10.150	0.577	0.998	Exit
10.714	0.485	0.843	Static Pressure 1.00 ATM
11.278	0.371	0.686	
11.841	0.226	0.528	
12.405	0.048	0.368	
12.510	0.010	—	
12.609	—	0.310	
12.725	0.157	0.157	

Fig. 6, Schematic of the low speed cascade wind tunnel, controlled-diffusion compressor blade and test conditions

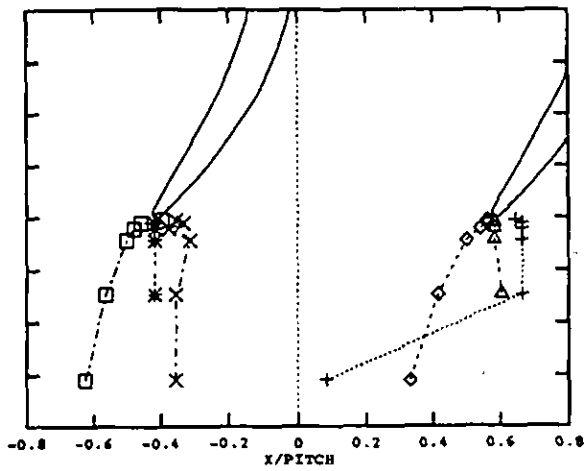


Fig. 7, Inlet flow angle = 43.3 deg.

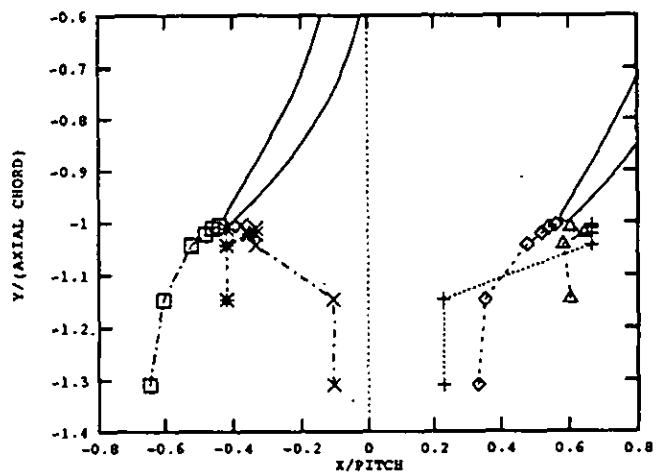


Fig. 8, Inlet flow angle = 46.4 deg.

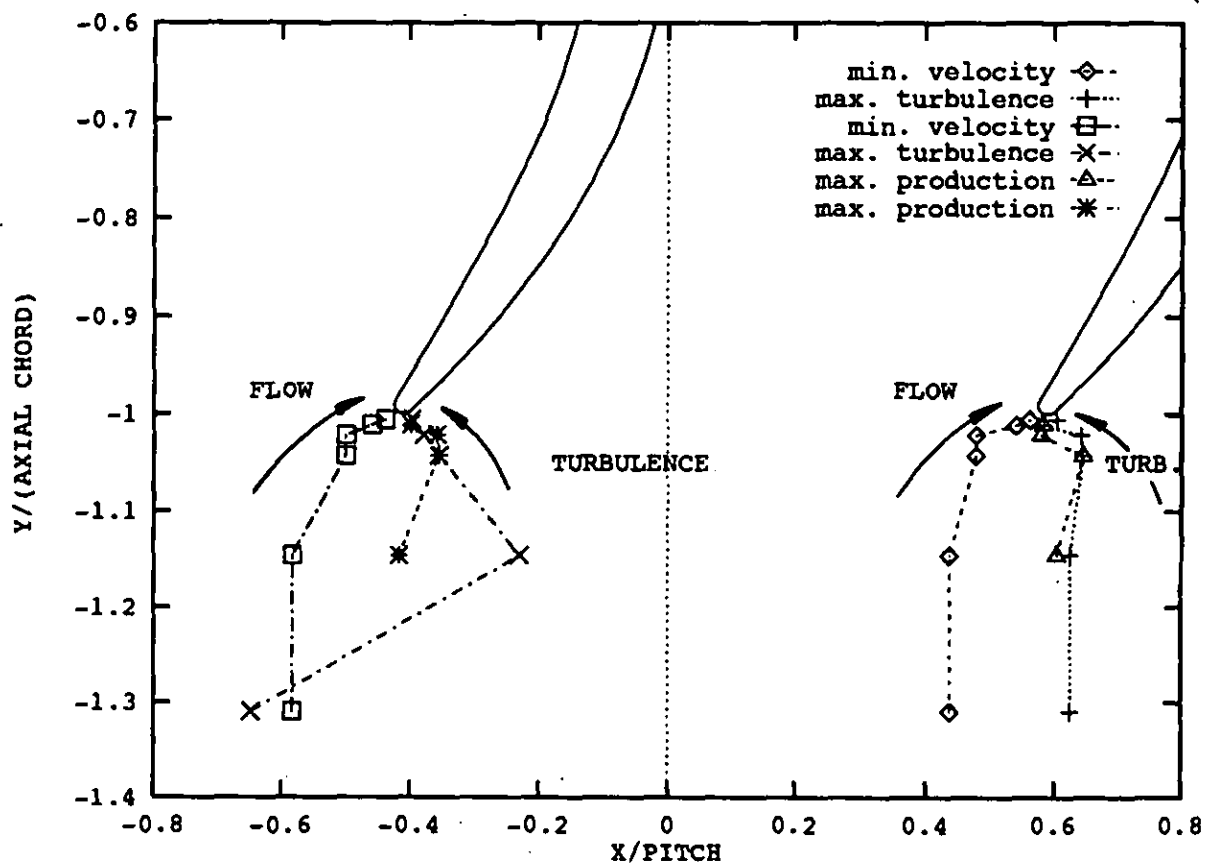


Fig. 9, Inlet flow angle = 48.4 deg. (Figs. 7, 8 & 9, Locus of points of min. total velocity, max. turbulence and max. turbulence production)

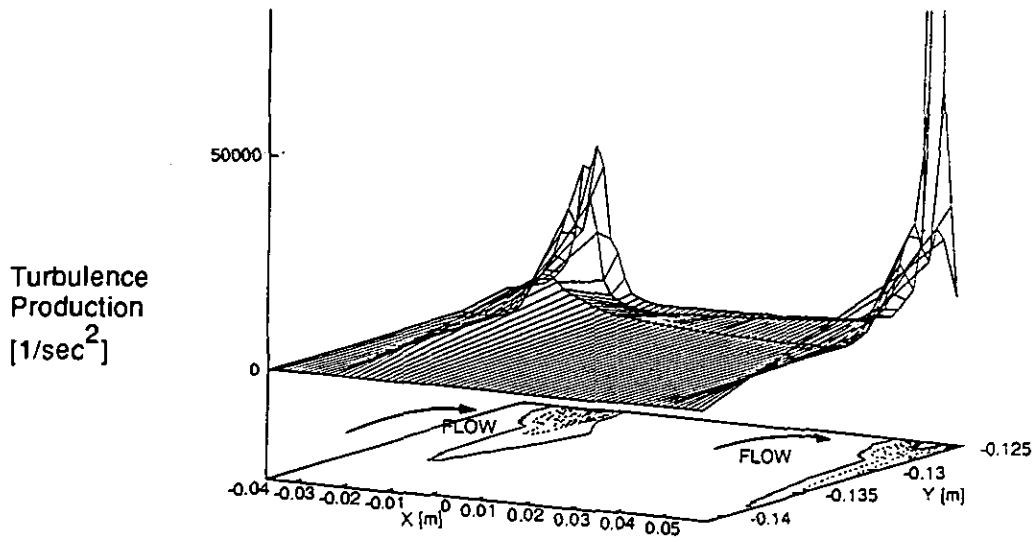


Fig. 10, Upstream turbulence production for 48.4 deg. inlet flow angle

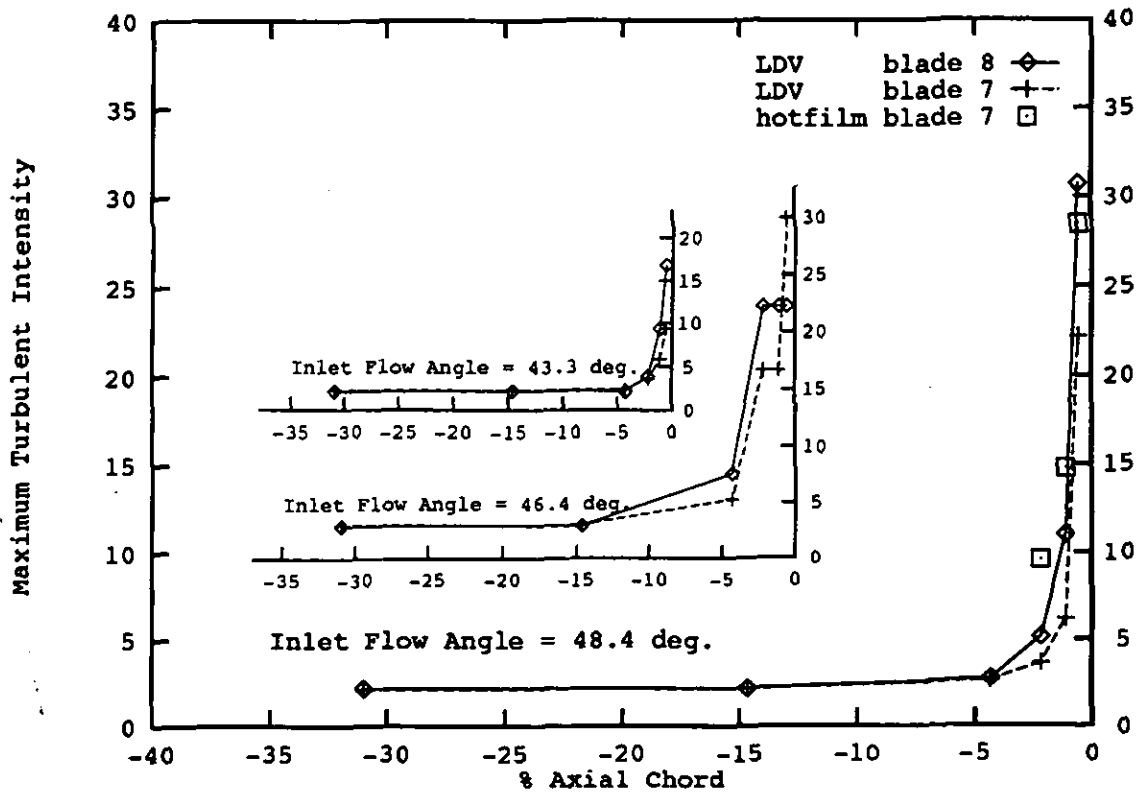


Fig. 11, Maximum inlet turbulence intensity for varying inlet flow angle

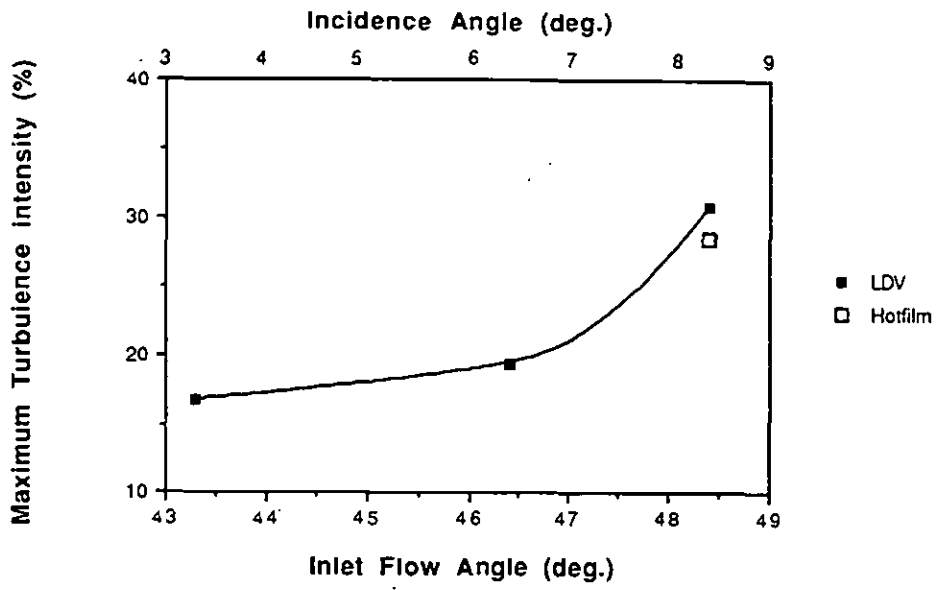


Fig. 12, Maximum cascade inlet turbulence (Re = 700 000)

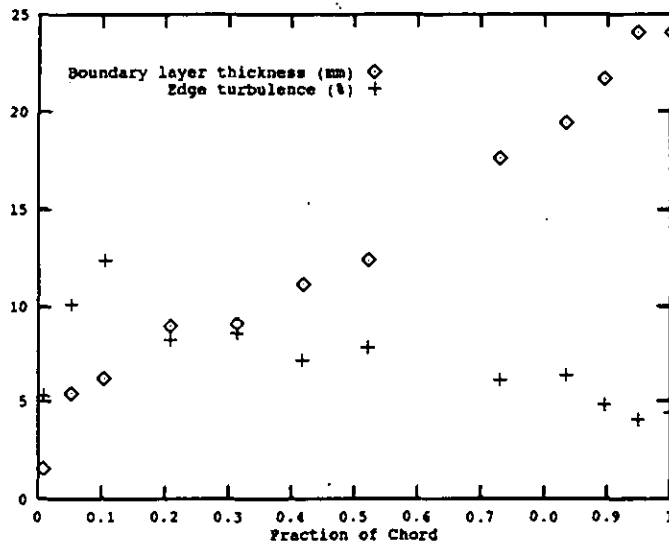


Fig. 13, Boundary layer thickness and variation of edge turbulence on the suction side at 48.4 deg. inlet flow angle